

A Hybrid Surrogate Intelligence Framework for Predictive Modelling and Proactive Optimisation of Wax Deposition in Crude Oil Flow Systems

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Abstract

This study presents a hybrid surrogate intelligence framework for the predictive modeling and optimization of wax deposition in crude oil flow systems. A comprehensive experimental dataset was generated from flow loop and cold finger tests to capture the interdependent effects of thermodynamic, hydrodynamic, and compositional parameters—namely flow velocity, pressure, temperature difference, wax appearance temperature, wax content, oil viscosity, and asphaltene concentration—on wax layer thickness. Two surrogate modeling techniques were developed and comparatively evaluated: Response Surface Methodology (RSM) employing a Custom Design matrix, and Artificial Neural Networks (ANN) trained using Levenberg–Marquardt (MLP-LM) and Bayesian Regularization (MLP-BR) algorithms. The RSM model facilitated parametric interpretation and statistical sensitivity analysis, while the ANN models provided high-fidelity nonlinear prediction capabilities. Optimization was achieved through RSM integrated with desirability functions (RSM-DF) and ANN coupled with a Genetic Algorithm (ANN-GA). The ANN-GA approach, particularly the MLP-BR-GA configuration, demonstrated superior performance, yielding a minimum predicted wax thickness of 0.223 mm compared to 0.385 mm from the RSM-DF model. Statistical evaluation confirmed the dominance of the MLP-BR architecture, with $R^2 = 0.9918$, $RMSE = 0.3275$, and $MAPE = 0.1236$, underscoring its robustness and generalization ability. The results reveal that optimal flow assurance conditions are achieved under low-pressure (~ 3 MPa), moderate temperature gradients (~ 5 °C), and reduced oil viscosity (~ 2.4 cP). Overall, the hybrid ANN-GA framework outperforms classical RSM-based techniques in accuracy and adaptability, establishing an effective data-driven paradigm for proactive wax management in crude oil production systems.

Keywords: Wax deposition; Artificial Neural Network; Response Surface Methodology; Genetic Algorithm; Flow assurance.

1. Introduction

Wax deposition is among the most persistent and costly flow assurance challenges in crude oil production, particularly in deep onshore and offshore environments where ambient conditions promote the precipitation of paraffinic hydrocarbons from the produced crude. As the crude oil flows from the reservoir to the surface, its temperature decreases due to heat losses to the surrounding formation, casing, or seabed. When this temperature drops below the wax appearance temperature (WAT), the solubility of long-chain paraffin components—typically C18 to C36 alkanes—diminishes, leading to the nucleation and crystallization of solid wax. These wax crystals adhere to each other and to the pipe wall, forming a coherent and viscous layer that gradually thickens over time [1-2]. The deposit reduces the effective internal diameter of the tubing, increases pressure drop, decreases flow rate, and, in extreme cases, results in total plugging of the wellbore or flowline. Such outcomes cause production deferment, operational downtime, and significant economic losses due to the frequent need for cleaning, intervention, or well shut-in [3-4].

The phenomenon of wax deposition is controlled by a combination of thermodynamic, hydrodynamic, and compositional factors. Thermodynamically, wax formation begins when the balance between the liquid and solid phases of paraffinic components is disturbed, and the temperature at which this occurs defines the WAT [5]. Below this temperature, solid wax crystals form and begin to separate from the liquid phase. Hydrodynamic factors, including flow velocity, shear rate, and turbulence intensity, influence the extent of deposition, as they govern the balance between deposition and removal mechanisms [1-2]. Under high-velocity turbulent flow, shear forces tend to prevent excessive buildup by promoting re-entrainment of crystals back into the flow stream, while in laminar or low-velocity regimes, deposition dominates due to insufficient shear. Compositional factors such as crude oil wax content, resin-to-asphaltene ratio, and viscosity determine the nature and strength of the wax network that forms [6]. Oils rich in high-molecular-weight paraffins tend to form stronger crystalline networks that trap large amounts of liquid, resulting in gel formation and severe flow restriction [7].

The mechanism of wax deposition is inherently complex because it involves coupled heat, mass, and momentum transfer phenomena. Initially, molecular diffusion is the dominant mechanism, as dissolved wax molecules migrate from the warmer core of the flow to the colder pipe wall driven by a concentration gradient. As the temperature difference between the bulk oil and the wall increases, the diffusion flux intensifies, causing accelerated deposition [4]. Once a layer of wax forms, it acts as an insulating barrier, further decreasing the wall temperature and promoting more precipitation. The deposit thickens until a steady-state condition is achieved, where the rate of deposition equals the rate of shear removal. However, variations in production rate, temperature, or composition continuously disturb this equilibrium, resulting in cyclic deposition and removal behavior [1]. Other contributing mechanisms include Brownian motion of small crystals, shear dispersion that enhances particle transport, and gravitational settling of heavier wax particles, especially in inclined or horizontal wells [8].

The formation of wax deposits adversely affects production efficiency and equipment integrity. The reduced flow area increases pressure losses and elevates the load on artificial lift systems such as electrical submersible pumps (ESPs) or gas-lift valves. The increased power demand can lead to premature pump failures or gas-lift instability [9]. In subsea systems, where maintenance access is limited, wax plugging can lead to prolonged downtime and costly remediation operations using remotely operated vehicles (ROVs) or pigging units [3]. The economic implications are profound, as de-waxing activities—whether thermal, mechanical, or chemical—require substantial investment. Moreover, the recurrence of wax deposition in wells that are frequently shut-in or experience transient flow conditions creates a recurring cost burden, often running into millions of dollars annually for large offshore operations [2].

The available mitigation and remediation strategies for wax deposition can broadly be classified into thermal, mechanical, and chemical approaches. Thermal techniques, such as hot oiling and hot water circulation, are the most commonly employed. They involve pumping heated fluids into the wellbore to melt the deposited wax and restore flow capacity [3]. Although effective, these operations are energy-intensive, transient in effect, and can cause scaling or thermal fatigue of the tubing. Mechanical methods, including pigging, wireline scraping, and coiled tubing milling, physically remove the deposits but necessitate well shut-ins, which lead to production interruptions. In subsea and deviated wells, mechanical cleaning becomes operationally difficult and risky [1]. Chemical methods employ solvents, dispersants, or paraffin inhibitors that alter the crystallization behavior of wax molecules [6]. While these can delay deposition, their performance is strongly dependent on crude composition and environmental conditions. Furthermore, chemical treatments require continuous injection and monitoring, increasing operational complexity. These existing methods, although mature, share a critical limitation—they are reactive rather than proactive. Most de-waxing interventions are carried out after measurable production decline or pressure anomalies, by which time wax deposition has already impaired flow [10]. This reactive operational mode results in excessive maintenance frequency, high energy expenditure, and non-optimized use of resources.

Consequently, there has been a growing interest in predictive and preventive control strategies that rely on real-time data analysis and forecasting. The ability to predict when and

where wax will deposit within the production system can enable timely and optimized interventions, reducing downtime and improving cost efficiency [11]. Conventional predictive tools based on thermodynamic modeling and empirical correlations, however, have proven inadequate for practical field application. Thermodynamic models such as regular solution theory and solid solution models require extensive compositional data for each hydrocarbon component, which are rarely available [1]. They also assume equilibrium conditions, neglecting the transient effects of flow rate and temperature fluctuations. Empirical correlations, on the other hand, are derived under limited laboratory conditions and lack generalization capability when applied to diverse field environments. The multiphysics nature of wax deposition, with its strong nonlinear dependencies on temperature, pressure, flow regime, and crude composition, challenges the applicability of these classical methods [2].

Recent advances in data science and artificial intelligence (AI) have opened new possibilities for addressing such nonlinear, multivariate flow assurance problems through data-driven modeling. Machine learning (ML) approaches, in particular, offer powerful tools for pattern recognition, feature selection, and predictive modeling without requiring explicit physical equations [7,9]. By learning directly from historical and real-time production data, ML algorithms can infer hidden relationships between operational parameters and wax deposition outcomes. Algorithms such as Artificial Neural Networks (ANN), Support Vector Machines (SVM), Random Forests (RF), and Gradient Boosting Decision Trees (GBDT) have been successfully applied to analogous problems such as hydrate formation prediction, asphaltene precipitation, and corrosion rate forecasting [12-13]. These successes suggest a strong potential for machine learning to revolutionize wax deposition forecasting and intervention optimization in oil production systems.

Among these techniques, the Artificial Neural Network (ANN) stands out due to its ability to capture highly nonlinear interactions between multiple inputs and outputs [11]. ANNs mimic the human brain's learning process by adjusting the connection weights between neurons based on training data, enabling them to predict complex responses even under noisy and incomplete datasets. For wax deposition modeling, ANN can be trained using operational parameters such as flow rate, tubing pressure, temperature profile, oil viscosity, and wax appearance temperature to predict outputs such as wax layer thickness or deposition rate [13]. The model learns from historical data trends to forecast future deposition behavior under varying conditions. This predictive capability can be further extended by integrating the ANN model with optimization algorithms that recommend the most efficient and cost-effective de-waxing schedules based on predicted outcomes [2].

Despite these possibilities, the application of machine learning to wax deposition forecasting remains in its infancy, and several research gaps persist. Most existing studies focus on steady-state or laboratory-scale systems, using limited datasets and static variables [1]. Very few have addressed the transient and dynamic nature of wax deposition under real field conditions where parameters vary continuously. Furthermore, previous models have primarily targeted prediction alone, neglecting the operational decision-making aspect of when and how to intervene. There is also a scarcity of models that generalize well across different wells and crude oil types, as most machine learning implementations remain case-specific. Data-driven models for wax deposition must also contend with challenges such as sparse datasets, variable sampling frequencies, and the need for feature normalization, which have not been adequately explored in earlier works [9,11]. Consequently, there is a clear need for a robust and generalizable predictive framework that integrates machine learning-based forecasting with optimization of intervention strategies, using readily available production data.

Response Surface Methodology (RSM) represents another powerful surrogate modeling approach widely applied in process optimization and prediction. RSM combines statistical and mathematical techniques to model and analyze the relationships between multiple input variables and one or more output responses. It is particularly effective for developing empirical correlations and identifying optimal operating conditions with a relatively small number of experimental runs. For wax deposition studies, RSM can be employed to quantify the combined effects of parameters such as flow velocity, pressure, temperature gradient, and crude oil composition on wax thickness or deposition rate, while generating response surfaces that

facilitate visualization and optimization of the process behavior [14]. When used alongside ANN, RSM serves as a complementary tool — offering interpretability and analytical precision that can validate or cross-check the results of data-driven models.

Despite these possibilities, the application of both machine learning and statistical surrogate modeling to wax deposition forecasting remains in its infancy, and several research gaps persist. Most existing studies focus on steady-state or laboratory-scale systems using limited datasets and static variables [1]. Very few have addressed the transient and dynamic nature of wax deposition under real field conditions where parameters vary continuously. Furthermore, previous models have primarily targeted prediction alone, neglecting the operational decision-making aspect of when and how to intervene. There is also a scarcity of models that generalize well across different wells and crude oil types, as most machine learning and RSM implementations remain case-specific. Data-driven models for wax deposition must also contend with challenges such as sparse datasets, variable sampling frequencies, and the need for feature normalization, which have not been adequately explored in earlier works [9,11]. Consequently, there is a clear need for a robust and generalizable predictive framework that integrates both machine learning-based forecasting and statistical optimization techniques such as RSM to develop reliable models and optimize intervention strategies using readily available production data.

This study presents a novel hybrid data-driven framework that addresses the longstanding challenge of developing a predictive and adaptive system for anticipating wax deposition and optimizing de-waxing operations in crude oil production systems. Traditional mechanistic and empirical models remain constrained by their deterministic formulations, reliance on detailed compositional data, and limited adaptability to dynamic field variations. Current operational practices—often reactive and schedule-based—lead to suboptimal wax management, resulting in increased downtime, higher maintenance costs, and reduced production efficiency. To overcome these limitations, the present research introduces an integrated surrogate modeling framework that combines Artificial Neural Network (ANN) and Response Surface Methodology (RSM) approaches for both prediction and optimization of wax deposition phenomena. The framework employs multilayer perceptron (MLP) ANN architectures trained on comprehensive field-scale and experimental datasets encompassing thermodynamic, hydrodynamic, and compositional parameters such as flow velocity (V_f), pressure (P), temperature difference (ΔT), wax appearance temperature (TWAT), wax content (W_c), oil viscosity (μ_o), and asphaltene content (A_c). The MLP-ANN is implemented using two distinct training algorithms—the Levenberg–Marquardt (LM) and Bayesian Regularization (BR)—to assess comparative performance in terms of generalization capability and prediction accuracy.

Furthermore, an RSM-based model is developed using a custom experimental design matrix to establish empirical relationships between the input variables and the output parameter, wax thickness (δ_w). This statistical model facilitates visualization of the response surfaces and interaction effects among parameters, offering interpretability that complements the data-driven ANN approach. For optimization, two independent strategies are employed: the ANN-GA (Genetic Algorithm coupled with ANN) framework, which leverages the ANN's nonlinear predictive power within an evolutionary optimization scheme to identify optimal de-waxing schedules and operating conditions; and the RSM-DF (RSM with Desirability Function) method, which simultaneously maximizes or minimizes multiple response targets based on defined desirability criteria. A comparative evaluation is conducted between the ANN-based and RSM-based models for both modelling accuracy and optimization efficiency, using statistical metrics such as R^2 , RMSE, MAE, and MAPE. This dual-modelling strategy enables cross-validation of predictive robustness and optimization performance.

2. Surrogate modelling of wax deposition

Surrogate modelling has emerged as a powerful alternative to mechanistic and purely empirical approaches for predicting wax deposition in crude oil transport systems. These data-driven or semi-empirical models approximate the underlying physics using statistical and machine learning methods, enabling rapid prediction and optimisation with reduced

computational cost. Among the most widely applied surrogate techniques are the Artificial Neural Network (ANN) and the Response Surface Methodology (RSM).

2.1. Artificial Neural Networks (ANNs)

ANNs have emerged as powerful computational modeling tools for addressing complex nonlinear relationships in petroleum production systems, particularly in the prediction and control of wax deposition phenomena in oil pipelines and wellbores [15]. Wax deposition is a highly nonlinear process influenced by multiple interacting parameters such as flow velocity, system pressure, temperature gradient (ΔT), wax appearance temperature (WAT), wax content, oil viscosity, and asphaltene concentration, all of which collectively govern wax precipitation, crystal growth, and deposition thickness. Traditional empirical or mechanistic models often fail to accurately capture these intricate relationships due to uncertainties in flow dynamics and thermodynamic conditions. In contrast, ANNs provide a robust data-driven framework capable of learning and modeling these dependencies directly from experimental or field data [16].

An ANN structured as an interconnected network of artificial neurons organized in layers, consisting of an input layer, one or more hidden layers, and an output layer, represents a Multilayer Perceptron (MLP) architecture, which is a type of feedforward neural network (FFNN). In this configuration, data flows in a single direction from the input layer through the hidden layers to the output layer without any feedback connections [17]. Each neuron processes the incoming signals through weighted connections, applies an activation function to introduce nonlinearity, and passes the transformed signal to the next layer. The network is typically trained using the backpropagation (BPNN) algorithm, which iteratively updates the connection weights based on the difference between the predicted and target outputs, minimizing this error through gradient descent or advanced optimization techniques such as the Levenberg–Marquardt (LM) or Bayesian Regularization (BR) algorithms. For example, in wax deposition modeling, the input neurons represent key operational and fluid parameters such as flow velocity (V), pressure (P), temperature difference (ΔT), wax appearance temperature (WAT), wax content (WC), oil viscosity (μ_o), and asphaltene content (AC), while the output neuron corresponds to the predicted wax layer thickness (Wt) under specific flow and thermal conditions [18].

Mathematically, the output of the n th neuron in the input or hidden layer is expressed as the weighted sum of all input signals plus a bias term, formulated as:

$$z_n = \left(\sum_{i=1}^k w_{ij} x_i \right) + b_n \quad (1)$$

where z_n is the net input to the n th neuron; w_{ij} represents the connection weight between the i th input and the n th neuron; x_i denotes the i th input variable; b_n is the bias associated with the neuron; and k is the total number of inputs. This weighted summation serves as the neuron's internal activation potential, which is then passed through an activation (or transfer) function to generate the neuron's output response.

The transfer (activation) function then transforms z_n into a nonlinear output signal f_n , defined as:

$$f_n = f(z_n) \quad (2)$$

Different transfer (activation) functions can be used depending on the level of nonlinearity present in the modeled system. In wax deposition modeling, which involves complex thermo-hydraulic and compositional nonlinear interactions, the tangent sigmoid (tansig), log-sigmoid (logsig), and pure linear (purelin) functions are widely adopted because of their smooth differentiability and their capability to represent nonlinear mappings during training. These functions are mathematically expressed as follows.

For tangent sigmoid:

$$f(x) = \frac{2}{1 + e^{-2x}} - 1 \quad (3)$$

For Log-sigmoid

$$f(x) = \frac{1}{1 + e^{-x}} \quad (4)$$

For pureline:

$$f(z) = z \tag{5}$$

The selection of these activation functions depends on the data normalization method: tan-sig is best suited for inputs normalized within the range of -1 to 1 , logsig works effectively for data scaled between 0 and 1 , and purelin is typically applied in the output layer for regression problems where a linear relationship between the processed signals and the output is anticipated. The hidden layer neurons compute nonlinear transformations of the inputs, thereby capturing intricate dependencies among the parameters affecting wax deposition [15]. The output of each hidden layer neuron h_j is thus given by:

$$h_j = f_h \left(\sum_{i=1}^k w_{ij} x_i \right) + b_j \tag{6}$$

where f_h denotes the activation function (typically tansig or logsig); and w_{ij} represents the weight between input neuron i and hidden neuron j . The output neuron aggregates the transformed signals from the hidden layer and applies an output transfer function, often linear for regression tasks such as wax thickness prediction: $\hat{y} = f_o(\sum_{i=1}^k w_{jo} x_i) + b_o$

where f_o is the output activation function (commonly purelin); w_{jo} is the weight connecting hidden neuron j to the output neuron; and \hat{y} represents the network-predicted wax thickness.

The training process iteratively adjusts all weights (w_{ij} , w_{jo}) and biases (b_j , b_o) to minimize the deviation between predicted and measured wax thickness values. The training of the ANN for wax deposition modeling is executed using numerical optimization algorithms designed to minimize a loss (error) function, typically defined as the Mean Squared Error (MSE):

$$E = \frac{1}{2N} \sum_{p=1}^N (y_p - \hat{y}_p)^2 \tag{8}$$

where y_p is the actual measured wax thickness; \hat{y}_p is the ANN-predicted value; and N is the number of training samples.

The Levenberg–Marquardt (LM) algorithm is one of the most efficient training methods for nonlinear process models such as wax deposition. It combines the speed of the Gauss–Newton algorithm with the stability of gradient descent, making it particularly effective for medium-sized networks with smooth error surfaces. The LM algorithm minimizes the cost function by adjusting weights according to:

$$[\Delta w = -(J^T J + \lambda I)^{-1} J^T e] \tag{9}$$

where J is the Jacobian matrix of partial derivatives of the network errors with respect to weights; I is the identity matrix; λ is the damping factor; and $e = y - \hat{y}$ represents the error vector between measured and predicted wax thickness values.

The Jacobian matrix J is expressed as:

$$J = \frac{\partial e}{\partial w} \tag{10}$$

The weight update rule is then:

$$w^{(k+1)} = w^{(k)} + \Delta w \tag{11}$$

The damping factor (λ) in the Levenberg–Marquardt (LM) algorithm is dynamically adjusted during the training process—decreasing when the model’s performance improves and increasing when the prediction error grows. This adaptive control enables a seamless transition between the Gauss–Newton method, which offers rapid convergence near the optimal solution, and gradient descent, which provides stability when the system is far from the minimum. Consequently, the LM algorithm delivers highly efficient convergence for nonlinear modeling tasks such as wax deposition prediction, where the relationships between process variables are complex, multivariate, and data-dependent [19].

In contrast, the Bayesian Regularization (BR) method incorporates probabilistic regularization to enhance model generalization and mitigate overfitting—an essential consideration in wax deposition studies where available training data are often sparse or affected by measurement noise. BR modifies the conventional error function by adding a regularization term that penalizes large network weights, thus favoring smoother mappings and reducing sensitivity to

outliers. This balance between model accuracy and complexity allows BR-trained networks to maintain predictive robustness across varying flow, thermal, and compositional conditions encountered in pipeline wax deposition modeling.

$$E = E_D + \alpha E_W \quad (12)$$

where: E_D is the data error term (mean squared error)

$$E_D = \frac{1}{2} \sum_{i=1}^n (y_i - \hat{y}_i)^2 \quad (13)$$

where, y_i is the target output; and (\hat{y}_i) is the network output for the i -th training example.

E_W is the weight decay term (sum of squares of the weights)

$$E_W = \frac{1}{2} \sum_{j=1}^m w_j^2 \quad (14)$$

where, (w_j) represents the weights of the network; and α is the regularization parameter that governs the balance between accurately fitting the training data and minimizing the magnitude of the network weights.

During the training process, Bayesian Regularization (BR) automatically adjusts α and other related hyperparameters to maximize the model evidence, thereby identifying the simplest ANN architecture that can effectively represent the wax deposition behavior. Through this adaptive mechanism, the BR-trained ANN achieves enhanced robustness and generalization capability, allowing it to accurately predict wax layer thickness across a wide range of operating conditions, even when the available data are sparse or noisy [20]. This characteristic is particularly valuable in field-scale wax deposition modeling, where variations in crude composition, flow velocity, and temperature gradients are prevalent, and many mechanistic parameters cannot be directly measured or validated experimentally.

Several studies have employed artificial neural-networks (ANNs) to model wax deposition phenomena with promising accuracy but varying methodological limitations. For example, Xie & Xing [19] used a radial-basis-function neural network (RBF-NN) to predict wax-deposition rate in crude-oil pipelines based on four key influencing factors; they achieved strong fit metrics though the dataset was small and lacked field-scale validation. Jalalnejhad & Kamali [21] developed an adaptive-network-based fuzzy inference system (ANFIS, hybrid of fuzzy logic + ANN) to predict wax deposition thickness under single-phase turbulent flow conditions, reporting excellent R (0.9929) and low deviation error (~ 0.0157) but faced limitations around narrow input conditions and lack of multiphase flow generalisation. Chen [22] applied a feed-forward ANN to model wax deposition rate for waxy crude oil pipelines, integrating experimental data and achieving low average relative error; yet the study still lacked development of a mechanistic linkage to asphaltene interactions and pressure effects. Kim *et al.* [23] proposed an AI-based model (including ANN elements) to predict both the location and amount of wax in oil pipelines using sensor and experimental inputs, showing good agreement with laboratory/field data but being constrained by limited oil types and pipe geometries. Jin *et al.* [24] developed a machine-learning based ANN model to predict wax deposition thickness on pipe walls from experimental loop data, achieving very low error metrics but still confronted limitations tied to dataset size and uncertain field transferability. Obaseki *et al.* [25] used dynamic modelling to predict wax deposition in pipelines, incorporating ANN elements alongside dynamic simulation, highlighting the nonlinear behaviour of deposition but showing that transient multiphase effects were not fully captured.

2.2. Response surface methodology

Response Surface Methodology (RSM) is a systematic and efficient suite of statistical and mathematical techniques for building empirical models of a response (output) as a function of several input (factor) variables, and for using those models to explore, visualize and optimize the response. In the context of wax deposition modelling - where the response of interest is wax thickness and the key input factors are flow velocity (m/s), pressure (MPa), ΔT ($^{\circ}C$), WAT ($^{\circ}C$), wax content (% wt), oil viscosity (cP) and asphaltene content (% wt). RSM offers a

pragmatic way to replace costly or time-consuming physical experiments by a fitted polynomial model that captures main, interaction and curvature effects, and then to use that model for prediction, sensitivity analysis and optimization of operating conditions to reduce wax build-up [26].

The standard RSM workflow begins with experimental design. For seven continuous factors a full two-level factorial design (2^7 runs) would be exhaustive but often impractical; therefore, practitioners typically use fractional factorials to screen for important factors, followed by a second-order design centered on the active factors. Common second-order designs are the Central Composite Design (CCD) and the Box–Behnken Design (BBD). A CCD for k factors typically consists of a 2^k factorial or fractional factorial portion, $2k$ axial (“star”) points at levels $\pm\alpha$ for each factor to enable estimation of curvature, and several replicates at the design center to estimate pure error. Levels are usually coded to scaled variables x_i where $x_i = (X_i - X_{0,i}) / \Delta_i$, with $X_{0,i}$ the center point and Δ_i the half-range so that coded levels are conveniently comparable across factors.

With the experimental design in place, the experiments are conducted by systematically varying the input factors according to the selected design matrix. For each combination of factor levels, the corresponding wax thickness is measured and recorded. Maintaining consistency, accuracy, and precision in data collection at this stage is essential to ensure the reliability and statistical validity of the results. For example, different combinations of flow velocity, system pressure, temperature differential (ΔT), wax appearance temperature (WAT), wax content, oil viscosity, and asphaltene content are tested, and the corresponding wax deposition thicknesses are obtained [26]. This provides the data foundation for developing a predictive and optimization model for wax formation under varying production and thermal conditions.

The next step involves constructing a mathematical model that quantitatively describes the relationship between the selected input factors and the response variable—wax thickness. In RSM, this is typically achieved by fitting the experimental data to a polynomial regression model that approximates the underlying physical relationship between the parameters. The models generally include linear, interaction (two-factor interaction, 2FI), and quadratic terms to capture both main and combined effects [27]. The general form of the models for linear regression is given as

$$y = a_0 + \sum_{i=1}^k a_i x_i + e \tag{15}$$

The general form of the 2FI regression model is given as

$$y = a_0 + \sum_{i=1}^k a_i x_i + \sum_{i < j} a_{ij} x_i x_j + e \tag{16}$$

The general form of the quadratic regression model is given as

$$y = a_0 + \sum_{i=1}^k a_i x_i + \sum_{i < j} a_{ij} x_i x_j + \sum_{i=1}^k a_{ii} x_i^2 + e \tag{17}$$

where x_i, x_j, x_l , are the input variables and a_i, a_{ij}, a_{ii} , and a_{ijl} are the coefficient of each of the terms, a_0 is the offset and e is the residual or error term.

The coefficients are estimated using regression analysis techniques, typically through the least squares method implemented in statistical software such as Design-Expert, Minitab, or MATLAB. The fitted polynomial model thus serves as a surrogate empirical representation of wax deposition behavior.

Following model development, statistical analysis is performed to evaluate the adequacy, validity, and reliability of the regression model. The most important analytical tool in this context is Analysis of Variance (ANOVA). ANOVA is used to assess both the overall significance of the developed regression model and the individual influence of each factor and interaction term on wax thickness. It decomposes the total variability of the response into components attributable to the model and to residual (unexplained) error. A small p -value (typically <

0.05) indicates that the regression model or an individual factor is statistically significant in influencing wax formation [27]. ANOVA also reveals significant interaction effects—for example, how the combined effect of flow velocity and ΔT influences the rate or thickness of wax deposition, which may differ from their individual contributions.

In addition to ANOVA, the estimated regression coefficients are statistically tested to determine their significance and contribution to the model. Each coefficient reflects the magnitude and direction of the relationship between its corresponding factor and the response. The linear terms describe direct effects (e.g., increasing flow velocity may reduce wax thickness), the interaction terms capture coupled effects (e.g., the combined influence of viscosity and WAT), and the quadratic terms represent curvature effects in the response surface [26]. These fitted terms allow the quadratic RSM model to accurately reproduce the nonlinear behavior typically observed in wax deposition phenomena.

Once the model has been statistically validated, its adequacy is further verified through model diagnostic checks. Important statistical indicators include the coefficient of determination (R^2), the adjusted R^2 , and the predicted R^2 . The R^2 value indicates the proportion of the total variation in wax thickness that is explained by the model, while the adjusted R^2 corrects for the number of predictors included, penalizing overfitting. Additionally, a lack-of-fit test is performed to determine whether the fitted model sufficiently captures the experimental data trends. A non-significant lack-of-fit ($p > 0.05$) confirms that the model is appropriate within the tested region. Residual analysis is also conducted to verify model assumptions; the residuals (differences between observed and predicted wax thickness values) should be randomly distributed and approximately normal. If residuals show systematic patterns, the model may need refinement, such as transformation or inclusion of additional terms.

After the model adequacy is confirmed, response surface and contour plots are generated to visualize the relationships between key factors and wax deposition. These graphical tools provide an intuitive means of understanding the interaction between two variables while holding others constant. A 3D response surface plot shows how the wax thickness changes as two factors vary, revealing peaks or valleys that correspond to maximum or minimum deposition. For instance, increasing flow velocity and decreasing ΔT may jointly minimize wax deposition, reflecting the dominance of shear-induced wax removal at high turbulence. Contour plots, which are 2D projections of the response surfaces, depict lines of constant wax thickness and are valuable for identifying operational regions that yield minimal wax buildup [27-28].

Once the response surfaces are established, optimization is performed to identify the factor settings that achieve the desired response objective—typically, minimizing wax thickness. The optimization can be carried out using either analytical or numerical approaches. In direct optimization, the polynomial regression model is solved to find the stationary point (minimum or maximum) of the response surface. Alternatively, desirability analysis can be used, especially when multiple performance objectives must be balanced, such as minimizing wax deposition while maintaining acceptable flow velocity and pressure drop. In this approach, each response is assigned a desirability function ranging from 0 (undesirable) to 1 (fully desirable), and the overall desirability function is maximized to identify optimal conditions that represent the best trade-off among competing criteria [26].

The final stage of the RSM-based modeling process is model validation. This involves conducting additional experiments at the predicted optimal levels of the input factors to verify the accuracy of the model's predictions. For wax deposition modeling, the predicted wax thickness at optimal operating conditions is compared to experimental measurements obtained under the same conditions. A close agreement between the predicted and observed values confirms that the developed RSM model is both valid and reliable. Conversely, significant deviations may indicate the need for model refinement, possibly by expanding the experimental domain or incorporating higher-order effects [27]. This validation step is crucial for ensuring confidence in the model's predictive capability and its applicability for real-field operations.

Through this systematic RSM framework, wax deposition behavior can be quantitatively modeled and optimized based on measurable operational and compositional parameters. The approach enables identification of the most influential factors—such as ΔT , flow velocity, and

wax content—and their synergistic effects on deposition dynamics. More importantly, it allows for determination of the optimal operational window that minimizes wax buildup, thereby improving flow assurance and reducing maintenance costs in oil production systems [28].

Ridzuan *et al.* [14] applied Response Surface Methodology (RSM) using a rotatable Central Composite Design (CCD) to optimize wax deposition measured with a cold-finger apparatus; they treated cold-finger temperature and experimental duration as the two coded factors, fitted a second-order polynomial (after a log transformation) and used ANOVA to validate the model, reporting the fitted model $\ln(\text{wax deposit} + 0.02) = -0.19 + 0.15B - 1.03A - 7.338e-03 AB + 0.033B^2 - 0.35A^2$ and showing excellent agreement between predicted and observed values with a verified minimum wax deposit of 0.0042 g at the optimized conditions; their study demonstrates RSM's strength for efficient experimental reduction and sensitivity analysis but is limited by the two-factor scope (so interactions with other operational variables like flow or composition were not examined) and by cold-finger lab conditions that reduce direct field transferability.

Salam, *et al.* [29] investigated paraffin-wax deposition in pipeline flow by screening and then modelling key operating parameters (temperature differential, flowrate and residence time) with a Box–Behnken RSM design to develop a quadratic regression surrogate; their ANOVA and model diagnostics returned strong predictive statistics (Pred $R^2 \approx 0.9618$ and Adj $R^2 \approx 0.9945$) and the model predicted a minimum wax deposit of 0.0195075 g at temperature = 53.25 °C, flowrate = 499.54 mL/min and residence time = 3.01 min, demonstrating that temperature, time and certain squared and interaction terms dominate deposition behavior; the work's main contribution is a validated empirical model usable to navigate the design space for mitigation, while its limitations include confinement to the tested ranges, reliance on laboratory flow rigs (limiting multiphase and large-scale applicability) and omission of compositional complexities that occur in real crude systems.

Adeyanju and Oyekunle [30] used a fabricated flow-loop rig to study wax deposition in sub-cooled pipeline conditions and applied Central Composite Design (CCD) RSM to quantify main and interaction effects of wall (coolant) temperature, inlet oil temperature, wax inhibitor concentration and oil flowrate on deposit volume; their model showed good fit between predicted and experimental values (predicted R-squares in reasonable agreement with adjusted R^2) and reported substantial reductions in deposit volumes across laminar and transition regimes (with predictive errors ~4–5%), enabling identification of significant terms (A, B, C, D and various interactions) for targeted mitigation; however, being a conference experimental study, limitations include restricted dataset size, specific crude/inhibitor types (which constrain generalisability), and the typical lab-to-field scaling uncertainty for pipeline systems.

Elganidi *et al.* [31] applied RSM (CCD) to optimise the synthesis parameters of a novel polymeric pour-point depressant/flow improver intended to control wax deposition, modelling the effect of reaction temperature, time and initiator concentration on polymerisation yield; their quadratic regression model produced $R^2 = 0.9696$ and identified optimal polymerisation conditions (reaction time ≈ 8.1 h, temperature ≈ 102 °C, initiator ≈ 1.57 wt%) that yielded a predicted maximum polymer yield of 93.75%, which experimental validation runs confirmed with an average yield of 93.20% (error $\approx 0.55\%$); while this study demonstrates how RSM can efficiently optimise wax-inhibitor production with strong statistical validation, limitations include that the study addresses additive synthesis rather than in-pipe deposition dynamics directly, and that the effectiveness of the synthesised polymer as a field inhibitor requires further flow-loop and field validation under diverse crude and thermal conditions.

3. Model simulation

In this study, both RSM and ANN models were employed as surrogate modeling tools to capture and predict the complex nonlinear behavior of wax deposition under varying flow and thermodynamic conditions. Surrogate models serve as efficient mathematical approximations of experimentally observed systems, enabling rapid prediction and optimization without requiring extensive laboratory or field testing. The RSM model provided an interpretable, statistically driven framework capable of describing quadratic relationships among the seven input

factors, while the ANN model offered superior flexibility in learning nonlinear and multidimensional interactions that govern wax formation and growth. By integrating these two complementary modeling techniques, the study established reliable predictive relationships between the input parameters—flow velocity (V_f), pressure (P), temperature difference (ΔT), wax appearance temperature (TWAT), wax content (W_c), oil viscosity (μ_o), and asphaltene content (A_c)—and the response variable, wax thickness (δw). The use of RSM and ANN as surrogate models thus provided a comprehensive and computationally efficient approach for understanding, predicting, and optimizing wax deposition behavior in pipeline flow systems.

3.1. Data preparation

A comprehensive experimental dataset was developed to establish and validate the proposed wax deposition prediction models. The database consists of 150 experimental observations obtained from a series of controlled flow loop and cold finger experiments, designed to simulate wax deposition under representative pipeline operating conditions. In these experiments, a synthetic crude oil system of known composition was circulated through a temperature-controlled stainless steel flow loop, enabling precise control of flow velocity, pressure, and temperature gradient between the bulk fluid and pipe wall. The extent of wax deposition was quantified by periodically measuring the wax layer thickness (δw , mm) on the inner pipe surface using laser micrometry and gravimetric analysis, following procedures similar to those recommended in standard flow assurance testing protocols.

The selected input parameters encompass the major thermophysical and compositional factors governing wax precipitation and growth dynamics. These include flow velocity (V_f , m/s), pressure (P , MPa), temperature difference (ΔT , °C) between bulk oil and wall surface, wax appearance temperature (TWAT, °C), wax content (W_c , %), oil viscosity (μ_o , cP), and asphaltene content (A_c , %). Each experiment was conducted under steady-state conditions to ensure reliable measurements of deposition thickness. The output variable, wax thickness (δw , mm), represents the overall measure of deposition severity and is the primary response used for model development and optimization. The resulting dataset provides a robust basis for correlating the complex nonlinear relationships between the thermodynamic, rheological, and compositional properties of crude oil systems and the observed extent of wax deposition.

3.2. ANN modelling

ANN models were developed using MATLAB to predict the nonlinear relationship between the governing process variables and the extent of wax deposition. The experimental data obtained from the controlled flow loop and cold finger tests were used as the input dataset for the modeling. The ANN development and simulation were carried out using MATLAB's Neural Network Toolbox (nntool), which offers multiple training algorithms and transfer functions for optimizing predictive accuracy.

A feed-forward multilayer perceptron (MLP) network based on the backpropagation learning principle was adopted to model the complex interactions among the process parameters. Two training algorithms were implemented and compared: the Levenberg–Marquardt (LM, `trainlm`) and the Bayesian Regularization (BR, `trainbr`) methods. The LM algorithm was evaluated for its fast convergence and suitability for smaller datasets, while the BR algorithm was tested for its strong generalization capability and reduced risk of overfitting.

The network structure consisted of seven input neurons, representing flow velocity (V_f , m/s), pressure (P , MPa), temperature difference (ΔT , °C), wax appearance temperature (TWAT, °C), wax content (W_c , %), oil viscosity (μ_o , cP), and asphaltene content (A_c , %). A single output neuron corresponding to wax thickness (δw , mm) was used to capture the wax deposition response. The hidden layer employed a tangent sigmoid (TANSIG) transfer function to account for nonlinear relationships, while a pure linear (PURELIN) function was used at the output layer to ensure continuous-valued predictions.

Multiple network topologies with hidden neuron numbers ranging from 5 to 20 were examined to identify the configuration that produced the best prediction accuracy. The dataset was randomly divided into training (70%), validation (15%), and testing (15%) subsets to ensure

unbiased model evaluation. Model performance was assessed using statistical indicators including the correlation coefficient (R), coefficient of determination (R^2), mean squared error (MSE), root mean squared error (RMSE), mean absolute error (MAE), and mean absolute percentage error (MAPE). Figure 1 shows the topology of the ANN model

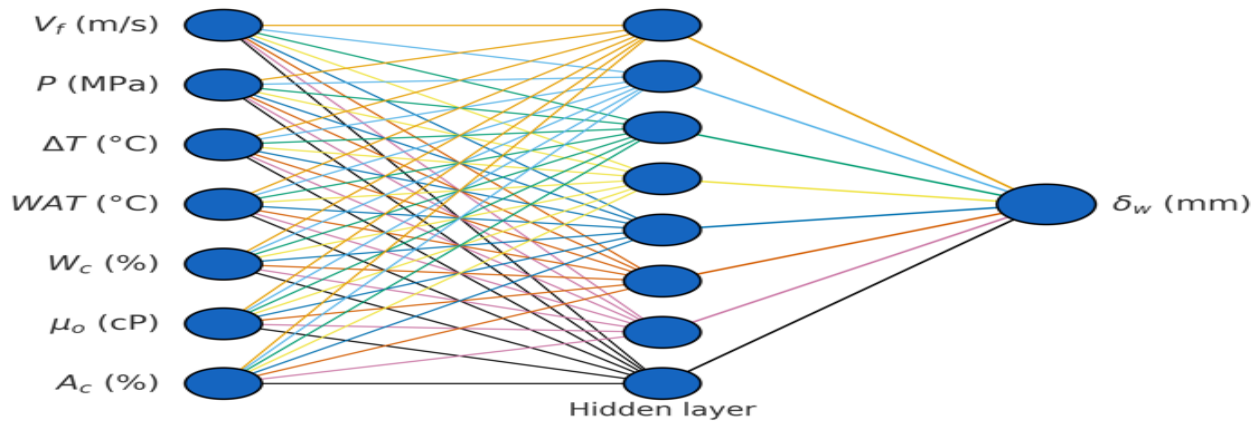


Figure 1. ANN topology for wax deposition.

3.3. RSM modelling

The experimental data obtained from the controlled flow loop and cold finger tests served as the foundation for the Response Surface Methodology (RSM) modeling of wax deposition. A Custom Design model was implemented using Design-Expert software (version 13) to establish quantitative relationships between the key input parameters and the wax thickness response. The custom design approach was adopted for this study due to its flexibility in accommodating non-standard experimental configurations and unequal factor levels, making it particularly suitable for complex flow assurance systems such as wax deposition processes.

Seven independent variables were considered as input factors: flow velocity (V_f , m/s), pressure (P , MPa), temperature difference (ΔT , °C), wax appearance temperature (TWAT, °C), wax content (W_c , %), oil viscosity (μ_o , cP), and asphaltene content (A_c , %). The wax thickness (δ_w , mm) was selected as the output response variable representing the extent of wax deposition under various operating conditions. The RSM model was generated based on experimentally measured data, and multiple regression models—including linear, two-factor interaction (2FI), and quadratic models—were evaluated to determine the most statistically significant representation of the experimental results. Model performance was assessed using statistical criteria such as the coefficient of determination (R^2), adjusted R^2 , predicted R^2 , standard deviation, and coefficient of variation (COV). Among these, the quadratic model provided the best fit for predicting wax thickness, effectively capturing the nonlinear interactions among the studied parameters. The final RSM model, developed through the Design-Expert platform, enabled the prediction and optimization of wax deposition behavior across the experimental domain.

3.4. Model optimisation

The wax thickness (δ_w) was optimized using two distinct modeling approaches: The Response Surface Methodology (RSM) combined with desirability factors (DF), and the Artificial Neural Network (ANN) coupled with a Genetic Algorithm (GA). These two optimization strategies were implemented to identify the operating conditions that minimize wax deposition while maintaining realistic flow and thermodynamic constraints.

For the RSM optimization, the built-in numerical optimization algorithm in Design-Expert software was employed. The optimization was guided by the defined desirability functions, where wax thickness (δ_w) was set as the response to be minimized, while the input parameters—flow velocity (V_f), pressure (P), temperature difference (ΔT), wax appearance

temperature (TWAT), wax content (Wc), oil viscosity (μ), and asphaltene content (Ac)—were optimized within their respective experimental ranges. The desirability-based optimization produced multiple candidate solutions, from which the most desirable point was selected based on the highest composite desirability value. In parallel, the ANN-GA hybrid optimization was conducted using the MATLAB GA toolbox, where the trained ANN model served as the fitness function for the genetic algorithm. The GA iteratively adjusted the input parameters to minimize the predicted wax thickness, leveraging the ANN’s nonlinear predictive capability and GA’s global search efficiency. The combination of both methods provided a robust comparative framework—RSM-DF for statistically driven optimization and ANN-GA for intelligent global search—to identify the most favorable operating conditions for minimizing wax deposition.

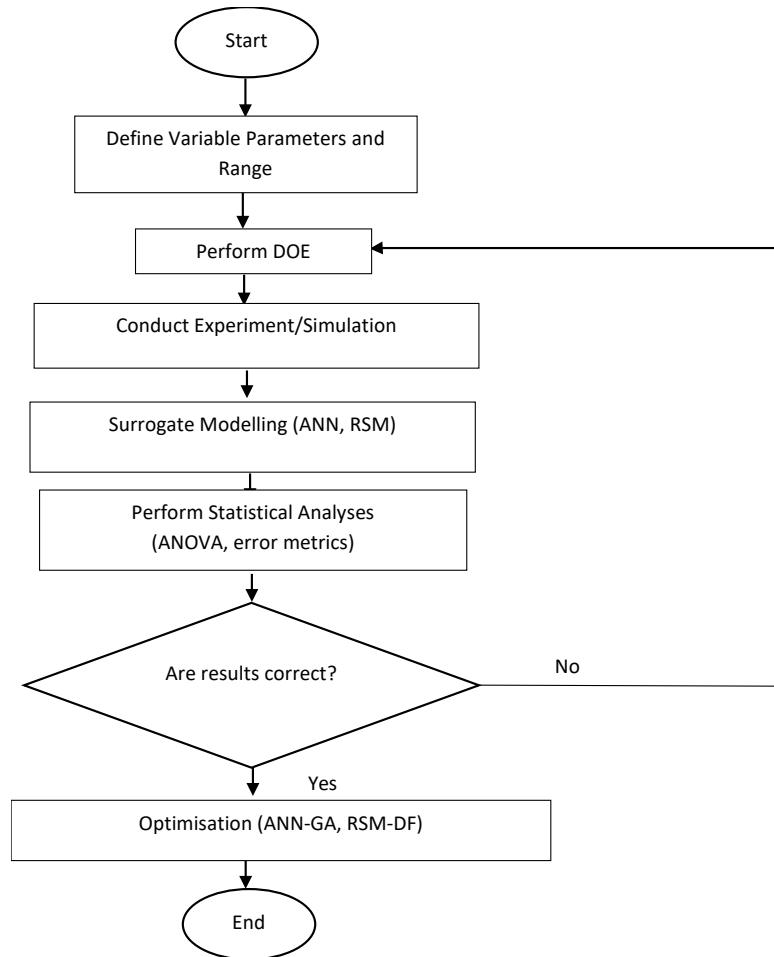


Figure 2. Flowchart of surrogate modelling and optimization.

3.5. Model performance metrics

Several statistical performance metrics were employed to evaluate the predictive accuracy of the developed RSM and ANN models. These include the coefficient of determination (R^2), mean squared error (MSE), root mean squared error (RMSE), mean absolute error (MAE), mean absolute percentage error (MAPE), and standard deviation (SD). The mathematical expressions for these evaluation parameters are presented below.

$$R^2 = \frac{\sum_{i=1}^n (x_{a,i} - x_{p,i})^2}{\sum_{i=1}^n (x_{p,i} - x_{a,ave})^2} \quad (18)$$

$$MSE = \frac{1}{n} \sum_{i=1}^n (x_{p,i} - x_{a,i})^2 \quad (19)$$

$$RMSE = \sqrt{\frac{1}{n} \sum_{i=1}^n (x_{p,i} - x_{a,i})^2} \quad (20)$$

$$MAE = \frac{1}{n} \sum_{i=1}^n |(x_{a,i} - x_{p,i})| \quad (21)$$

$$MAPE = \frac{\frac{1}{n} \sum_{i=1}^n |(x_{a,i} - x_{p,i})|}{\frac{1}{n} \sum_{i=1}^n x_{a,i}} \quad (22)$$

$$std\ dev = \sqrt{\sum_{i=1}^n \frac{(x_{di} - m)^2}{n - 1}} \quad (23)$$

where n is the number of experimental runs; xp,i is the estimated values; xa,i is the experimental values; xa,ave is the average experimental values; x_{di} is the difference between the actual and estimated value; m is the mean value of x_d dataset; k is the number of input variables.

4. Results and discussion

4.1. Results for ANN modelling

The ANN model result shown in Figure 3 displays the regression plots of ANN training, validation and testing for MLP-LM and MLP-BR. Figure 3a shows the result for MLP-LM while figure 3b shows that for MLP-BR.

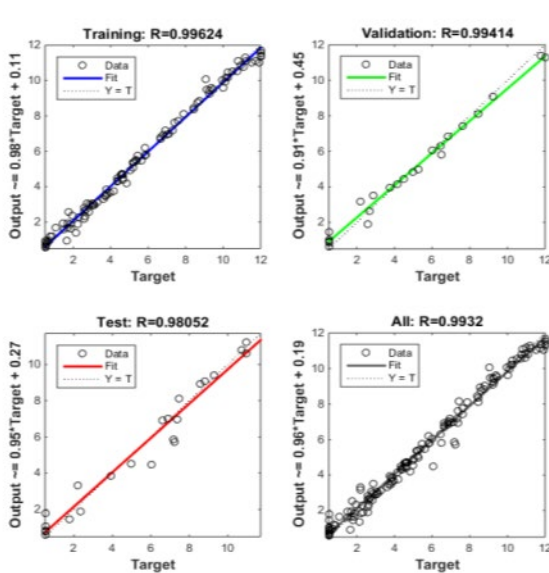


Figure 3a. R values for MLP-LM.

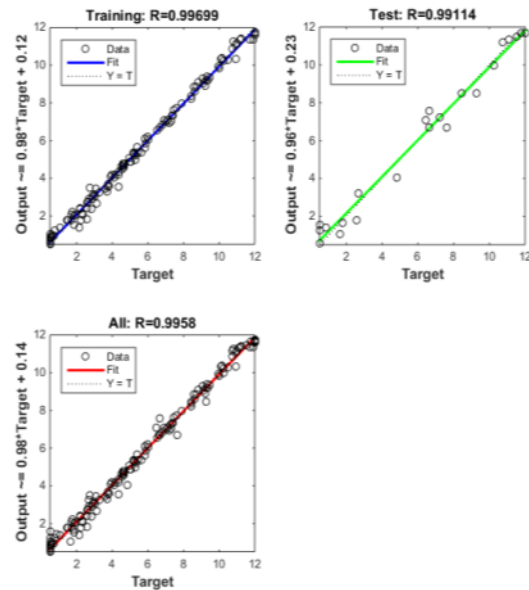


Figure 3b. R values for MLP-BR.

Figure 3 presents the correlation coefficients (R-values) for the two ANN models trained using the MLP-LM and MLP-BR algorithms. Both training algorithms achieved exceptionally high R-values, exceeding 0.99, which indicates a very strong correlation between the predicted and experimental wax thickness values. Specifically, the MLP-BR model exhibited a slightly higher R-value of 0.9958 compared to 0.9932 for the MLP-LM model, suggesting that the Bayesian Regularization algorithm achieved better generalization and fitting accuracy. This superior performance is attributed to BR's ability to automatically regulate the network's complexity during training, minimizing overfitting while maintaining high predictive precision. The

high R-values for both models confirm that the ANN architectures effectively captured the nonlinear relationships among the process variables governing wax deposition, with MLP-BR demonstrating marginally improved robustness and reliability. The performance plots of the ANN trainings are given in Figure 4.

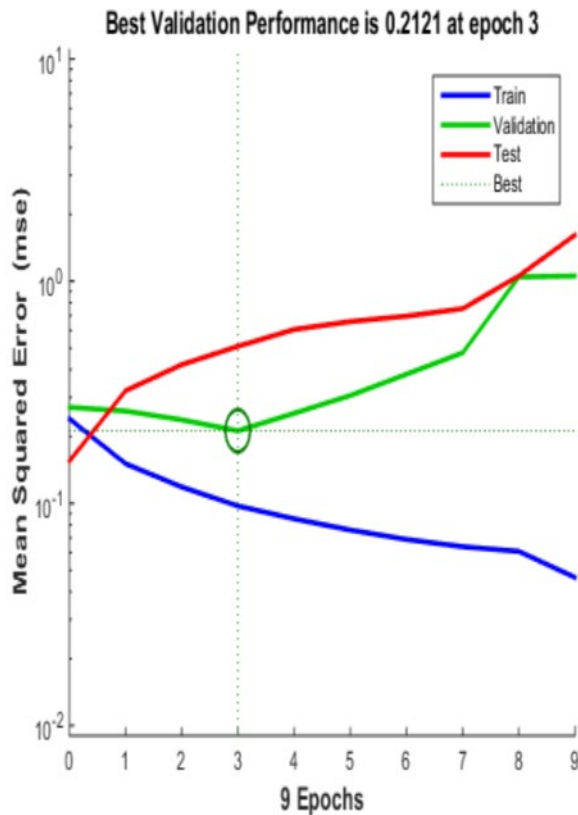


Figure 4a. MSE values for MLP-LM

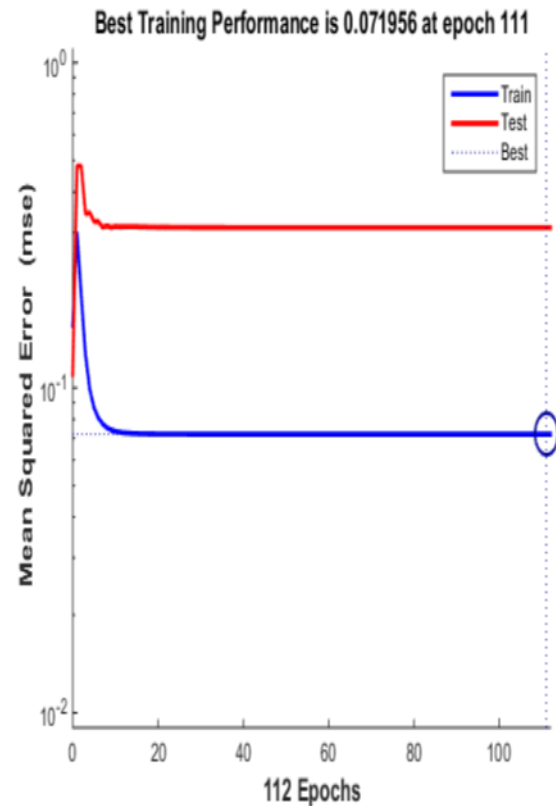


Figure 4b. MSE values for MLP-BR

The performance plots presented in Figure 3 illustrate the mean squared error (MSE) evolution during the training of the two multilayer perceptron (MLP) architectures—MLP-LM (Figure 4a) and MLP-BR (Figure 4b). Both networks demonstrate effective convergence, indicated by a consistent reduction in MSE as the training progresses. For the MLP-LM model, convergence was achieved after 9 epochs, with the minimum validation error of 0.2121 observed at epoch 3, beyond which further iterations did not significantly improve performance, suggesting early stabilization and prevention of overfitting through optimal weight adjustment. Conversely, the MLP-BR model exhibited a more gradual learning process, converging after 112 epochs, with the lowest validation MSE of 0.071956 recorded at epoch 111.

The notably lower MSE and extended training duration of the MLP-BR indicate its superior generalization capability and robustness, as the Bayesian Regularization algorithm inherently minimizes overfitting by incorporating a regularization term that balances the network's complexity and predictive accuracy. This contrasts with the Levenberg–Marquardt (LM) algorithm, which typically converges faster but may yield slightly higher residual errors when dealing with noisy or highly nonlinear datasets. Hence, while both models successfully captured the nonlinear relationships between the input parameters and wax deposition thickness, the MLP-BR architecture demonstrated a more stable and accurate learning performance, making it better suited for predictive modeling of complex, multivariate wax deposition behavior.

4.2. Results for RSM modelling

The RSM model results demonstrate the relationship between the independent process variables — flow velocity (V_f , m/s), pressure (P , MPa), temperature difference (ΔT , °C), wax appearance temperature (WAT, °C), water cut (W_c , %), crude oil viscosity (μ_o , cP), and asphaltene content (A_c , %) — and their collective influence on the wax layer thickness (δw , mm). Among the regression models evaluated, the Two-Factor Interaction (2FI) model provided the best fit to the experimental data (see Table 1), exhibiting the highest predictive accuracy and statistical significance. This model effectively captures the nonlinear interactions between key operational and compositional parameters influencing wax deposition in multi-phase flow systems. The RSM-derived model (equation 24) mathematically represents the predictive relationship between the seven independent variables and the resulting wax deposition thickness, enabling quantitative evaluation of how process adjustments — such as reducing ΔT , optimizing flow velocity, or modifying oil composition — affect wax buildup under varying production conditions. This model thus serves as a valuable analytical tool for optimizing flow assurance strategies and mitigating wax formation in crude oil transport pipelines.

$$\begin{aligned} \text{Wax Deposition (mm)} = & 5.6969 - 2.8498A - 0.186445 B + 3.10728C - 0.0178939D + 3.02636E + \\ & 1.96101F - 1.10973G - 0.143733AB - 0.444702AC + 0.0866813AD - 0.502335AE - 0.925202AF + \\ & 0.0519625AG + 0.162116BC + 0.0671215 BD - 0.274041BE - 0.0304305BF + 0.0384699BG - \\ & 0.0431437CD + 0.363462 CE + 0.335471CF - 0.0780947CG - 0.078076DE + 0.060703DF + \\ & 0.391363DG + 0.35808EF - 0.178346EG - 0.436057FG \end{aligned} \quad (24)$$

For Equations (24), the variables A, B, C, D, E, F, and G correspond to the seven key process parameters influencing wax deposition: flow velocity (A: V_f , m/s), pressure (B: P , MPa), temperature difference (C: ΔT , °C), wax appearance temperature (D: WAT, °C), water cut (E: W_c , %), crude oil viscosity (F: μ_o , cP), and asphaltene content (G: A_c , %). These equations are employed to predict the response — wax layer thickness (δw , mm) — at specified levels of each input variable. To ensure accurate predictions, all factor levels must be expressed in their original physical units for both the input parameters and the output response. This allows for precise quantitative interpretation and comparison with experimental or field data. To evaluate the statistical robustness and relative influence of each factor and their interactions, an Analysis of Variance (ANOVA) was conducted. The results, summarized in Table 2, include key statistical metrics such as degrees of freedom (DF), mean square (MS), F-values, and p-values for the model and its terms. In Table 2, the p-values (< 0.0001) and the corresponding high F-values confirm that the regression model is highly significant, indicating that variations in the selected input parameters have a strong and measurable effect on wax deposition thickness. This validates the reliability of the developed RSM-based predictive model for assessing and optimizing wax deposition behavior under varying flow and compositional conditions.

Table 1. Error data for RSM model analyses.

Source	Sequential p-value	Lack of Fit p-value	Adjusted R ²	Predicted R ²	
Linear	< 0.0001		0.9591	0.9561	
2FI	< 0.0001		0.972	0.9641	Suggested
Quadratic	0.5932		0.9716	0.9612	
Cubic	0.2096		0.9768	0.8481	
Quartic					Aliased

Table 2: RSM ANOVA

Source	Sum of squares	df	Mean square	F-value	p-value	
Model	1849.57	28	66.06	185.58	< 0.0001	significant
A-Flow velocity	296.04	1	296.04	831.71	< 0.0001	
B-Pressure	1.37	1	1.37	3.86	0.0518	
C- ΔT	430.27	1	430.27	1208.82	< 0.0001	
D-WAT	0.0146	1	0.0146	0.0409	0.84	
E-Wax content	370.01	1	370.01	1039.5	< 0.0001	
F-Viscosity	137.53	1	137.53	386.39	< 0.0001	
G-Asphaltene content	55.49	1	55.49	155.88	< 0.0001	
AB	0.2901	1	0.2901	0.8149	0.3685	
AC	3.69	1	3.69	10.36	0.0017	
AD	0.1125	1	0.1125	0.3161	0.575	
AE	3.4	1	3.4	9.55	0.0025	
AF	10.07	1	10.07	28.3	< 0.0001	
AG	0.0389	1	0.0389	0.1092	0.7416	
BC	0.4296	1	0.4296	1.21	0.2741	
BD	0.0651	1	0.0651	0.1829	0.6697	
BE	0.958	1	0.958	2.69	0.1035	
BF	0.0122	1	0.0122	0.0342	0.8535	
BG	0.0216	1	0.0216	0.0606	0.806	
CD	0.0305	1	0.0305	0.0857	0.7702	
CE	1.6	1	1.6	4.5	0.036	
CF	1.51	1	1.51	4.26	0.0413	
CG	0.1028	1	0.1028	0.2889	0.5919	
DE	0.0875	1	0.0875	0.2457	0.621	
DF	0.056	1	0.056	0.1574	0.6922	
DG	2.45	1	2.45	6.88	0.0098	
EF	1.61	1	1.61	4.53	0.0353	
EG	0.3798	1	0.3798	1.07	0.3037	
FG	2.66	1	2.66	7.47	0.0072	
Residual	43.07	121	0.3559			
Cor total	1892.64	149				

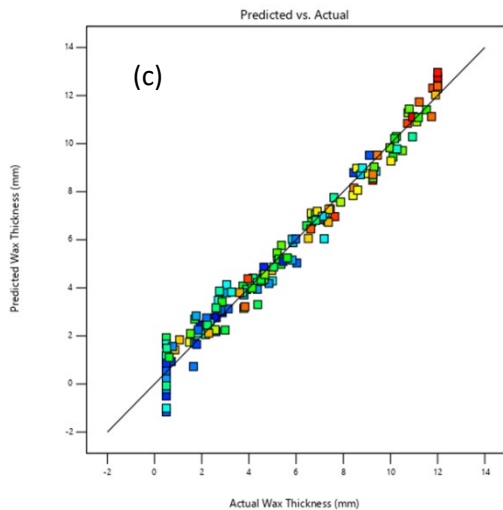


Figure 5. Parity plot of actual vs predicted values for wax thickness.

Figure 5 shows the actual vs. predicted response for the 2FI regression model.

Figure 5 depict parity plots illustrating the relationship between the actual and predicted responses for thickness. These figure demonstrate that the actual and predicted output responses closely align around the 45-degree line for all selected models, indicating strong regression and agreement between the two datasets. Thus, there exists an acceptable level of agreement between the actual experimental data and the predicted responses from the RSM models.

4.3 General performance metrics

Table 3 shows the comparison of performance metrics for the RSM and the ANN modelling. The comparative performance metrics for the MLP-LM, MLP-BR, and RSM models given in Table 3 reveal clear distinctions in their predictive capabilities for modeling wax deposition behavior. Among the three models, the MLP-BR architecture achieved the most accurate and consistent predictions, as evidenced by its lowest mean squared error (MSE = 0.1073) and root mean squared error (RMSE = 0.3275), alongside the highest coefficient of determination ($R^2 = 0.9918$). This indicates that the Bayesian Regularization network captured nearly all the variance between the experimental and predicted wax thickness values, achieving superior generalization with minimal overfitting. The Levenberg–Marquardt (MLP-LM) model also performed strongly, with MSE = 0.1781, RMSE = 0.4220, and $R^2 = 0.9864$, showing that it could approximate the nonlinear relationships among the input variables with high precision, though slightly less effectively than MLP-BR. This marginal difference can be attributed to the inherent differences in training algorithms—while LM converges faster and efficiently minimizes local error, BR introduces an adaptive regularization term that balances model complexity with fitting accuracy, making it more resilient to noise and data variability typical of experimental wax deposition datasets.

Table 3. Performance metrics for RSM and ANN predictions.

Metric	MLP-LM	MLP-BR	RSM
MSE	0.178097	0.107268	0.287253
RMSE	0.422015	0.327518	0.53596
MAE	0.299648	0.239721	0.421105
MAPE	0.154478	0.123596	0.252083
R2	0.98644	0.99175	0.97723

The RSM model, although demonstrating reasonable predictive ability with $R^2 = 0.9772$, was comparatively less accurate than the ANN-based models. Its MSE (0.2873), RMSE (0.5360), and MAE (0.4211) were higher, indicating greater deviation between predicted and actual wax deposition values. This outcome aligns with the inherent limitation of RSM as a second-order polynomial-based statistical approach, which assumes smooth, continuous response surfaces and may not fully capture the strong nonlinearities and complex interdependencies among parameters such as temperature differential, viscosity, and asphaltene content. In contrast, the ANN models—particularly MLP-BR—excel at representing such nonlinear, multivariable interactions due to their distributed learning and nonparametric structure.

Overall, these results demonstrate that ANN-based surrogate models significantly outperform RSM models in accurately predicting wax deposition trends under varying flow and thermodynamic conditions. The superior performance of MLP-BR further highlights the advantage of incorporating Bayesian Regularization in training neural networks for complex flow assurance problems, offering improved generalization and stability. Nonetheless, the RSM model remains valuable for providing interpretable parametric relationships and initial screening of key factors, while ANN models offer superior predictive power for dynamic and nonlinear wax deposition modeling.

4.4. Model optimisation

Table 4 presents the optimization results of the wax deposition modeling conducted using two advanced surrogate-based optimization techniques—Response Surface Methodology integrated with Desirability Function (RSM-DF) and Artificial Neural Network coupled with Genetic Algorithm (ANN-GA). The ANN-GA framework includes two ANN architectures, namely MLP-LM and MLP-BR, each trained and optimized separately to capture and minimize the wax layer thickness (δw , mm) under realistic flow and fluid property constraints. Both optimization strategies were designed to identify the most favorable operating conditions that minimize wax deposition while maintaining stable flow characteristics and crude oil properties. The seven independent variables considered were flow velocity (V_f), pressure (P), temperature difference

(ΔT), wax appearance temperature (WAT), water cut (Wc), oil viscosity (μ_o), and asphaltene content (Ac). The RSM-DF method employed a multi-objective desirability approach to generate several potential optimal points, with the best point determined by the highest composite desirability value (approaching 1.0), representing the most efficient condition for minimizing δw .

In parallel, the ANN-GA optimization was performed by coupling the predictive ANN models (MLP-LM and MLP-BR) with a Genetic Algorithm to achieve global optimization. The results demonstrate that the ANN-GA framework yielded lower optimal wax thickness values compared to RSM-DF, confirming its superior ability to capture nonlinear interactions among the process parameters and identify the true global optimum. Between the two ANN-GA configurations, the MLP-BR-GA exhibited the best performance, achieving the minimum δw value due to its enhanced generalization capability and robust learning characteristics. Overall, Table 8 provides a comprehensive summary of the optimization outcomes, illustrating how the integrated use of RSM-DF and ANN-GA (MLP-LM and MLP-BR) frameworks enables accurate identification of the optimal operating envelope for minimizing wax buildup. These results offer valuable insights for developing predictive control and flow assurance strategies in crude oil transport systems, supporting proactive wax management through data-driven optimization.

Table 4. Optimisation results.

Parameter	Symbol	Unit	RSM	MLP-LM	MLP-BR
Flow velocity	Vf	m/s	2.05	2.967	2.025
Pressure	P	MPa	13.73	3.061	3.041
Temperature difference	ΔT	$^{\circ}C$	11.88	5.379	5.243
Wax appearance temperature	TWAT	$^{\circ}C$	25.73	25.227	25.222
Wax content	Wc	wt%	1.29	1.281	1.280
Oil viscosity	μ_o	cP	16.46	2.454	2.43
Asphaltene content	Ac	wt%	0.24	0.231	0.230
Wax thickness (output)	δw	mm	0.385	0.227	0.223

The optimization of wax deposition parameters using RSM integrated with Desirability Functions (RSM-DF) generated multiple feasible solutions that satisfied the defined optimization objectives to varying degrees. From nearly one hundred computed optimal points, the most technically suitable and statistically consistent condition was selected based on both model accuracy and physicochemical relevance. The selected optimal condition (Table 4) corresponds to a flow velocity (Vf) of 2.05 m/s, pressure (P) of 13.73 MPa, temperature difference (ΔT) of 11.88 $^{\circ}C$, wax appearance temperature (TWAT) of 25.73 $^{\circ}C$, wax content (Wc) of 1.29 wt%, oil viscosity (μ_o) of 16.46 cP, and asphaltene content (Ac) of 0.24 wt%, resulting in a predicted wax layer thickness (δw) of 0.385 mm and a composite desirability value of 1.00. This optimal setting represents a balanced interaction between thermodynamic and hydrodynamic effects—where a moderate flow velocity maintains turbulent flow to suppress deposition, and a controlled temperature gradient limits wax crystallization and growth.

A comparative analysis of optimization outcomes from RSM-DF and Artificial Neural Network–Genetic Algorithm (ANN-GA) approaches (Table 4) highlights significant differences in predictive performance and solution quality. While RSM-DF successfully identified operating conditions that reduce wax accumulation, its quadratic polynomial structure inherently limits the accurate representation of nonlinear interactions among variables such as viscosity, flow rate, and temperature differential. Consequently, the RSM-derived optimum ($\delta w = 0.385$ mm) reflects a local minimum rather than a true global optimum in the complex multidimensional space of wax deposition behavior.

In contrast, the ANN-GA hybrid models, integrating Multilayer Perceptron (MLP) architectures with Levenberg–Marquardt (LM) and Bayesian Regularization (BR) training algorithms, achieved significantly improved results. The MLP-LM-GA and MLP-BR-GA frameworks yielded minimum wax thickness values of 0.227 mm and 0.223 mm, respectively. The superior performance of the ANN-GA models arises from their enhanced nonlinear learning capability and the global search efficiency of the genetic algorithm, which jointly enable accurate mapping and optimization of the complex relationships governing wax deposition.

The optimized parameter ranges identified by ANN-GA—pressure ≈ 3 MPa, temperature difference ≈ 5 °C, oil viscosity ≈ 2.4 cP, TWAT ≈ 25 °C, and $W_c \approx 1.28$ %—demonstrate that reduced pressure, lower viscosity, and moderate temperature gradients favor minimal wax buildup. These trends align with established flow assurance principles emphasizing rheological control and thermal management for deposition mitigation.

Overall, the results confirm that ANN-GA provides a more accurate and robust optimization framework than RSM-DF for predicting and minimizing wax deposition. While RSM-DF remains valuable for preliminary parameter screening and for offering interpretable parametric trends, the MLP-BR-GA model proved to be the most effective surrogate optimization tool, combining strong generalization capability with high predictive precision in modeling the nonlinear behavior of wax formation systems.

5. Conclusion

This study developed and evaluated a hybrid surrogate intelligence framework integrating Response Surface Methodology (RSM) and Artificial Neural Networks (ANN) for the prediction and optimization of wax deposition in crude oil flow systems. The modeling approach employed seven governing parameters—flow velocity (V_f), pressure (P), temperature difference (ΔT), wax appearance temperature (TWAT), wax content (W_c), oil viscosity (μ_o), and asphaltene content (Ac)—to predict the resulting wax layer thickness (δw).

Within the RSM framework, a Custom Design configuration was implemented, and regression analysis indicated that the Two-Factor Interaction (2FI) model provided the best statistical fit among all tested models. The 2FI model achieved high predictive accuracy with $R^2 = 0.972$ and Predicted $R^2 = 0.964$, effectively capturing significant interaction effects such as flow velocity– ΔT , ΔT –viscosity, and viscosity–asphaltene content. The Analysis of Variance (ANOVA) confirmed the strong statistical significance of ΔT , W_c , and μ_o ($p < 0.0001$), underscoring their dominant influence on wax formation. The RSM–Desirability Function (RSM-DF) optimization yielded an optimal operating condition characterized by $V_f = 2.05$ m/s, $P = 13.73$ MPa, $\Delta T = 11.88$ °C, TWAT = 25.73 °C, $W_c = 1.29$ wt%, $\mu_o = 16.46$ cP, and $Ac = 0.24$ wt%, resulting in a predicted wax thickness (δw) of 0.385 mm with a composite desirability of 1.00.

In contrast, the ANN models—developed using Multilayer Perceptron (MLP) architectures trained with Levenberg–Marquardt (LM) and Bayesian Regularization (BR) algorithms—demonstrated markedly superior predictive and optimization performance. The MLP-BR model achieved the best overall accuracy with $R^2 = 0.9918$, RMSE = 0.3275, and MAPE = 0.1236, outperforming both MLP-LM and RSM models. When coupled with a Genetic Algorithm (GA) for optimization, the MLP-BR-GA and MLP-LM-GA configurations yielded minimum wax thicknesses of 0.223 mm and 0.227 mm, respectively—representing a 42–43% reduction relative to the RSM-DF optimum. The ANN-GA results further indicated that lower pressure (~ 3 MPa), reduced viscosity (~ 2.4 cP), and moderate temperature gradients (~ 5 °C) favor minimal wax deposition, aligning well with established flow assurance principles.

Overall, the comparative results confirm that the ANN-GA hybrid framework offers a more robust and accurate predictive capability for modeling complex nonlinear behaviors governing wax deposition, whereas the RSM-2FI model remains valuable for preliminary screening and interpretation of key parameter interactions. The integration of these complementary surrogate modeling techniques thus provides both explainability and precision, establishing a reliable data-driven approach for proactive wax management. The developed MLP-BR-GA model represents the most effective surrogate optimization tool for minimizing wax buildup, providing a strong foundation for intelligent flow assurance systems capable of real-time prediction and operational optimization in crude oil production environments.

Appendix

Table A1: Training data and outputs

Flow Velocity (m/s)	Pressure (MPa)	ΔT (°C)	WAT (°C)	Wax content (%wt)	Oil viscosity (cP)	Asphaltene content (%wt)	Wax thickness (mm)			
							Actual	MLP-LM	MLP-BR	RSM
1.43635	13.89919	6.80886	40.54294	3.365091	13.45601	0.782082	Actual	MLP-LM	MLP-BR	RSM
2.876786	5.874743	23.59741	36.16808	4.900265	94.10355	0.27429	0.5	0.879231	0.869236	0.4044
2.329985	4.738738	23.92223	33.48444	3.478147	63.51539	0.708019	4.996136	4.830325	4.837347	4.29
1.996646	8.873433	27.31005	43.12709	2.241835	34.82075	1.832516	3.049267	3.065985	2.991799	3.8
0.890047	14.82781	30.4132	27.22395	2.688902	15.64866	1.379989	2.57101	2.191347	2.001494	2.77
0.889986	5.904663	39.15482	34.8525	7.450903	79.81447	2.699481	6.029865	4.468665	5.960845	5.03
0.645209	11.06563	23.07051	25.22707	3.888672	62.76713	2.488842	10.98117	11.21547	11.10603	11.12
2.66544	12.13944	16.30348	34.37321	6.099778	54.27919	1.157089	5.869948	5.82306	5.903145	5.88
2.002788	5.851651	32.83152	26.12607	8.047842	89.60147	0.926386	2.161964	1.380383	1.276882	2.05
2.270181	11.7386	14.47913	27.37636	10.66553	79.28253	1.263139	10.11201	9.955237	10.25304	9.45
0.551461	7.413398	20.364	27.35052	1.55037	16.86414	1.852826	5.245321	5.36921	6.269614	5.14
2.924775	10.58767	7.745973	37.98421	12.19175	32.54876	0.950578	2.620185	2.33934	2.759922	2.77
2.581107	10.60236	5.887276	39.9209	9.790605	26.35194	1.947617	1.059214	1.662457	1.250597	1.84
1.030848	9.429296	38.69269	36.66738	2.144626	74.90674	1.346353	0.5	1.054482	0.747766	0.79
0.954562	4.083477	34.2593	44.24345	13.2301	5.286179	1.745732	8.442661	8.086697	8.567451	8.79
0.958511	13.02363	29.3591	32.49741	13.89221	57.84919	1.421154	9.446158	9.507898	9.507509	9.52
1.260606	6.849361	19.31335	30.71424	1.855091	76.72095	1.024504	11.79329	11.38482	11.60739	12.31
1.811891	5.238222	11.0653	42.37198	4.876287	87.92303	2.855669	4.637804	4.495645	4.803568	4.86
1.579863	3.489302	10.4753	29.47192	12.28682	35.52401	2.338096	2.3502	1.899066	2.086384	2.54
1.228073	10.09072	13.7585	44.26445	11.47564	82.48322	0.592317	4.969786	4.543996	4.894846	4.73
2.029632	11.13077	24.22293	25.24309	3.583294	12.84191	2.63171	8.570466	8.934495	8.894145	8.97
0.848735	3.199054	30.01086	44.39758	3.930891	84.95232	1.564807	0.591042	0.763171	0.927809	1.37
1.230362	9.145117	28.10691	25.8632	6.186609	14.49389	2.704746	8.734556	8.842121	8.800946	8.71
1.415905	5.717949	14.79769	42.82286	7.783322	40.93415	2.439595	4.174948	3.764113	3.986026	4.41
1.640175	10.74207	38.42028	35.55402	9.655567	80.13495	1.390598	3.743878	3.945359	3.528747	4.07
2.46294	5.092397	30.82639	44.8593	6.164791	16.69191	0.262914	10.74431	10.80462	11.15372	11.28
0.999184	11.29125	24.40239	26.47593	7.475486	24.46664	0.952297	3.905793	3.830004	4.043881	3.93
1.785586	7.640824	26.41023	36.07709	11.46459	72.78075	1.716576	6.664981	6.783393	6.999232	6.74
1.981036	14.24076	19.686	44.38605	1.513565	72.56358	1.973739	9.062379	10.06694	9.274089	8.76

Flow Velocity (m/s)	Pressure (MPa)	ΔT (°C)	WAT (°C)	Wax content (%wt)	Oil viscosity (cP)	Asphaltene content (%wt)	Wax thickness (mm)			
0.616126	4.650251	13.67058	35.46196	4.534117	64.83247	0.922086	1.935164	2.358114	2.149209	2.45
2.018862	7.092796	17.45904	37.58797	10.98689	70.00695	0.590197	7.192466	5.849976	6.96647	6.04
0.92631	4.361682	31.52461	38.91497	13.5329	55.187	2.537805	6.64742	6.711714	7.139102	7.1
0.662629	14.09632	5.503772	34.09082	8.163484	26.67631	2.956326	11.2192	11.12982	11.33813	11.73
2.872214	13.52807	9.062542	37.55116	8.449589	35.87821	1.671933	2.183108	3.337091	2.373129	2.5
2.91408	6.0953	6.610092	36.68629	2.500408	19.79658	0.680702	0.5	1.024116	0.676979	0.4491
2.520993	10.91981	6.425508	43.02316	7.263773	91.02816	0.962461	0.5	0.76728	0.513753	-1.16
1.261534	12.80667	34.94112	25.90893	8.456642	59.1724	0.251494	2.990452	2.886324	2.789681	2.24
0.74418	9.66241	29.62803	30.61926	4.394587	41.28344	2.760037	11.53039	11.03333	11.4106	11.41
2.210583	9.355807	21.59608	44.00823	4.769405	47.27657	0.529703	5.833217	6.213122	5.973468	6.02
1.600381	5.902227	8.424196	42.80528	6.281978	94.83377	1.814246	2.701351	2.702421	3.108581	3.49
0.805096	4.117233	22.20656	34.11314	1.280997	17.02844	0.967355	4.350874	4.498318	4.349004	4.21
1.737942	13.76659	21.57151	37.40265	5.509108	59.45052	1.751698	2.870497	2.982568	3.01817	2.96
0.585971	13.80502	11.06207	30.54762	3.960272	51.57709	2.023977	4.611634	4.737024	4.689142	4.54
2.773301	10.59722	20.18481	28.76242	5.584963	61.92252	2.523277	3.788755	3.836827	3.637758	3.71
1.14695	7.068357	18.94767	34.27397	2.67667	3.774798	0.77798	0.5	0.856903	1.133596	1.17
2.156306	7.190515	26.55475	32.06704	13.46738	87.46814	0.230788	2.600602	1.87442	1.605609	2.18
1.279278	11.71147	27.22828	36.67312	9.310294	93.34759	0.58328	11.74059	11.12365	11.34665	11.12
1.80017	13.76532	6.58564	26.55469	10.50743	57.38305	2.720052	10.79697	11.11654	11.17381	11.44
1.866776	13.64504	18.11144	44.4879	12.0484	70.27178	2.646892	2.569679	2.613525	2.412992	2.26
0.962136	12.35851	26.9051	44.72421	7.978191	92.40494	1.872757	6.518556	5.820074	6.572325	6.06
2.923962	10.70438	22.60977	38.96323	2.216884	71.30939	1.881447	10.25404	10.45577	10.22372	10.3
2.437832	4.00968	34.97714	35.72193	8.519492	16.94883	2.062103	0.710076	0.95751	0.934117	0.9334
2.848747	4.939545	28.05428	31.19055	9.215776	58.47626	0.69104	5.363456	5.488266	5.163787	4.98
2.737068	13.78265	10.7027	41.2759	11.43615	61.45807	2.760353	5.379383	5.461574	5.698702	5.77
1.99475	10.27715	7.469906	38.69462	7.043234	43.56481	1.372557	1.481419	1.931244	1.723772	1.74
2.804686	3.110365	27.48467	28.25234	2.786124	74.17154	1.272788	0.5	1.782671	1.14403	1.93
0.721231	4.217659	5.927896	43.21854	4.972863	93.56797	1.65297	2.203165	3.171588	2.611	2.74
0.989957	10.96202	25.50215	41.45074	6.083152	92.70571	0.331505	5.208392	5.087999	5.31796	5.29
0.613068	3.060739	37.90806	43.996	10.04284	46.18226	0.665593	10.93447	10.8619	10.35144	10.29
1.313326	4.929697	25.1416	39.51439	8.990896	13.09733	2.266494	12	11.70425	11.64924	12.66

Flow Velocity (m/s)	Pressure (MPa)	ΔT (°C)	WAT (°C)	Wax content (%wt)	Oil viscosity (cP)	Asphaltene content (%wt)	Wax thickness (mm)			
1.471693	9.584805	18.58595	37.2683	5.985354	98.51444	0.431836	5.194018	5.346914	5.344591	5.45
1.178373	11.30274	27.51509	33.36486	14.81121	84.21201	1.888826	7.602675	7.743622	7.62958	7.76
2.571844	10.82354	21.03885	43.65457	9.480847	14.21694	0.886978	12	11.30731	11.61079	12.75
1.391883	5.691232	24.09659	42.32128	4.321175	92.2425	1.290028	3.783316	3.477413	3.519111	3.15
1.202336	11.54615	37.95127	25.90437	2.424955	87.24984	1.008342	6.814865	6.924168	6.856546	7.04
1.85674	5.846989	18.51359	25.52734	3.140028	52.84613	1.195884	9.107989	9.499943	9.013545	9.51
0.852311	6.904796	38.64167	32.52927	4.443408	59.94499	2.213329	2.838562	2.556856	2.432003	3.07
2.505492	11.9579	36.68727	41.21107	3.249539	41.10226	1.031941	9.386794	9.614291	9.173282	8.85
0.686377	10.79559	11.85269	44.74552	3.611938	7.366641	1.785933	4.851407	4.181793	4.493966	4.18
2.967217	13.19068	7.427646	28.00834	4.991332	34.84933	1.532941	1.692115	1.667782	1.876186	1.71
2.430612	10.89135	8.52723	36.88261	3.42723	80.67964	2.058279	0.5	0.549047	0.531244	-1.01
0.996789	9.819703	5.637764	32.61782	13.55472	2.453938	2.823123	0.5	0.616756	0.809562	0.2433
0.513805	4.124097	8.305504	44.39829	2.123272	34.68292	2.251202	3.831488	3.603663	3.163748	3.22
2.538654	7.41259	28.90524	41.84238	8.343159	41.02053	0.801833	1.781649	1.477785	1.784755	1.65
2.267143	6.182428	7.491603	41.76657	6.745556	54.66477	0.287313	5.26919	4.978641	5.155272	5.19
2.322518	5.927876	16.16415	34.37386	14.7533	92.14585	0.934339	2.239966	1.856024	1.734147	2.45
2.428176	14.67613	34.57064	33.29639	2.568545	35.94191	1.866218	9.247654	9.068285	9.166586	8.48
0.685112	7.717173	5.814518	30.46814	6.569978	36.00141	0.343992	3.12316	2.958712	2.988612	3.13
1.396164	13.70456	33.5064	26.12751	14.57259	74.27512	1.589825	4.584345	4.693802	4.675326	4.4
0.789673	10.57366	14.86492	42.29445	13.1171	46.31736	1.87116	12	11.55682	11.66911	12.96
2.657759	12.53774	9.135769	41.25802	12.43901	24.01127	1.135883	8.449648	8.365589	8.310554	8.15
2.058245	9.031645	29.3858	44.99435	4.61064	46.33907	2.358554	2.297374	2.293276	1.975703	2.11
1.327245	9.922847	27.013	44.93274	3.392426	15.80399	0.498475	3.058509	2.945483	3.92995	4.13
0.658896	8.910212	35.71152	36.10863	10.36101	19.28592	0.410386	4.356456	4.352933	4.373293	3.94
1.277456	5.342916	30.72749	40.37975	14.01126	50.84004	2.238929	11.11489	10.79486	11.21356	10.91
1.312958	11.66943	33.12183	43.89531	8.794681	43.05469	1.587376	10.72272	10.54877	10.80211	10.84
2.324015	6.369268	14.87121	41.99295	9.002578	91.6549	2.127527	9.261371	9.250297	9.248808	8.58
2.093894	3.291792	11.21038	29.94696	4.919707	37.5146	1.417517	4.641765	4.377003	4.624666	4.35
2.718032	10.74567	31.27152	34.01088	11.7729	58.89766	0.889926	0.5	0.907871	0.82061	1.66
1.680537	5.125328	33.23922	27.58319	3.618612	63.9619	2.493486	6.898688	7.032794	7.366768	7.18
0.798986	14.2855	39.66768	44.08102	5.531509	3.283257	2.438364	5.832239	5.778069	5.833359	5.16

Flow Velocity (m/s)	Pressure (MPa)	ΔT (°C)	WAT (°C)	Wax content (%wt)	Oil viscosity (cP)	Asphaltene content (%wt)	Wax thickness (mm)			
2.283112	14.44714	19.44162	37.12349	6.95611	67.02666	2.14515	7.23804	5.695956	7.259661	6.99
2.401963	13.97837	18.02063	29.57286	8.106545	19.44752	0.962006	4.375439	4.297606	3.762456	3.3
1.903193	7.441904	32.17445	38.43401	4.393736	96.18489	1.852646	1.701375	1.940315	1.872983	2.7
2.427418	3.185479	16.92812	37.36256	2.607716	16.56895	1.210727	7.310479	7.185266	7.114683	6.79
1.734489	14.13982	37.57651	32.16325	9.548681	42.63316	0.45643	0.5	0.924333	0.624553	0.5451
1.806832	8.13821	35.04445	27.27115	5.040828	10.36427	2.768478	10.50866	10.54385	10.28103	9.71
1.568853	14.59986	20.01479	38.43146	9.137335	99.69368	0.583092	3.268006	3.093692	3.383277	3.83
0.563548	14.56344	31.28049	35.40615	3.161078	51.21511	2.860665	9.307215	9.422221	9.3471	9.03
0.769729	13.23611	31.409	40.44637	7.735961	60.34773	1.448816	7.003939	6.959549	6.964218	6.85
0.578573	6.533387	8.609335	35.40327	8.456252	8.573495	0.718372	10.1771	10.20479	10.43519	10.21
2.091026	7.621173	36.58935	42.04363	1.72553	75.49613	1.717323	4.134321	4.135935	3.956635	3.99
1.28589	13.21364	22.68383	36.03814	5.71246	22.57075	2.644248	5.451063	5.758395	5.392606	5.1
1.771427	6.803064	33.92601	36.21876	2.881805	90.00932	2.25023	3.728226	3.452322	3.399844	3.8
2.768916	5.033913	16.20174	42.53307	1.88725	22.10368	2.458371	5.984563	6.032217	6.328191	6.03
1.123231	9.681615	36.34331	33.06966	14.85944	20.6874	2.044593	0.5	0.585398	0.528106	-0.4959
1.525957	14.23386	18.62206	27.6803	5.512954	5.581867	2.138374	10.93894	10.59715	11.06531	11.11
2.388878	11.35236	5.379318	25.57565	12.33824	48.26256	2.577748	1.831913	1.6289	1.524067	2.12
1.071995	9.840734	36.68837	40.10275	4.564969	57.35443	0.89907	0.862126	1.164781	1.228254	1.42
0.69245	4.166118	8.195034	37.40619	10.54104	8.439447	1.57039	8.809174	9.053498	9.141091	8.98
1.224379	10.38009	16.17598	39.0816	11.64319	78.00171	0.819386	4.532668	4.682343	4.502871	4.27
0.903053	14.88065	38.25217	29.25928	9.338942	46.42231	2.96547	10.02318	9.616021	9.77284	9.28
2.824244	4.681008	38.27125	27.72743	7.602067	53.39025	2.843366	9.978136	10.04455	9.833791	9.83
2.520301	9.219956	25.07033	25.29089	6.765773	45.19475	0.310395	4.511893	4.455147	4.557	4.33
2.083509	13.52848	27.1143	32.01175	5.884156	41.27478	2.17561	5.048199	4.924109	4.918513	4.87
2.678651	11.88922	20.69559	36.79835	14.01341	56.84475	2.790695	2.755409	3.052191	3.53959	3.86
2.50918	11.36419	15.26238	32.84488	12.62867	17.21354	0.705611	3.959472	3.644638	4.10692	4.38
0.966425	11.42981	16.50326	33.7495	14.51038	19.82896	1.790247	3.610056	3.316938	3.555701	3.81
2.731397	7.313894	28.53815	43.08317	2.740161	86.45499	2.763367	7.448001	8.13496	7.610018	7.29
1.848356	6.523102	31.33311	31.96511	11.23214	94.71932	0.295049	1.850655	1.860914	2.075597	2.26
2.5186	12.71233	32.70527	35.27979	14.13677	38.58431	2.152777	12	11.40111	11.66268	12.29
2.740228	12.72136	32.63663	40.67306	3.537263	28.53298	1.032577	7.64183	7.417016	6.671368	6.97

Flow Velocity (m/s)	Pressure (MPa)	ΔT (°C)	WAT (°C)	Wax content (%wt)	Oil viscosity (cP)	Asphaltene content (%wt)	Wax thickness (mm)			
1.295009	13.40487	8.192214	32.93086	1.930948	65.11196	2.788309	1.763936	2.546168	2.362861	2.84
0.77513	13.95889	22.30471	37.44173	11.37569	42.05595	2.918963	0.5	0.855938	1.05705	0.8659
1.069838	9.136109	7.014557	42.24727	9.042624	4.487863	2.843946	8.414818	8.464387	8.305523	7.84
1.567769	9.018196	24.23351	43.99041	12.7856	17.30295	1.5278	1.523965	1.577059	1.828605	2.1
2.545037	12.57954	20.45357	27.94147	2.956813	72.16528	2.613719	6.9134	7.201397	7.497226	6.85
2.651826	10.79957	36.06965	43.53175	12.13374	66.57455	2.564738	1.647135	0.93303	1.555357	0.7277
0.51738	11.4236	17.28203	34.84233	3.822782	4.655407	1.093481	7.393129	7.619035	7.409373	7.26
1.776868	12.54951	9.097346	30.16489	3.291183	23.75327	2.520963	2.669568	2.628096	2.672472	3.14
1.543528	13.68006	10.00471	34.18272	3.299721	24.64533	0.303621	0.5	0.646676	0.571066	-0.2056
1.05527	7.055942	31.65287	44.60065	12.40405	67.84549	1.869556	0.75856	1.201025	1.181635	1.56
0.799663	7.506995	26.63763	34.85236	10.31276	3.931633	0.844025	11.91272	11.02396	11.3335	12.02
1.344038	4.127783	8.539294	31.57503	8.322916	12.20264	0.537587	7.885492	8.112814	7.831426	7.57
2.857274	9.939362	7.943738	37.66802	6.023627	80.39178	0.415469	2.865312	3.513917	3.063853	3.42
1.308007	3.431307	29.53392	29.80291	13.28081	19.49738	2.149609	0.518819	1.44571	1.305382	1.49
1.796977	8.587176	7.546705	26.51727	6.494232	65.96912	1.15165	9.254234	9.459239	9.30126	8.71
2.257547	9.511736	33.7651	27.57759	12.43239	25.34191	2.229347	2.600076	2.830042	2.634325	3.17
1.409074	6.438495	29.71848	27.56092	7.147889	11.74526	0.382998	7.367614	6.9589	7.338225	6.73
2.929455	10.09	7.847207	28.03805	6.277222	25.83087	1.082813	6.447182	6.295778	6.26035	6.59
2.906118	3.366003	7.96932	27.77654	7.477517	72.78216	1.710576	0.5	0.677156	0.541598	-0.0716
1.129456	3.448178	39.53239	37.81749	5.21929	85.85825	2.414025	0.622858	0.852436	0.920525	1.11
1.743121	12.87121	18.09948	28.6376	11.46653	83.36155	1.092507	10.27803	10.19844	10.28494	9.78
1.252196	7.322288	17.97248	31.91335	8.038085	40.92399	1.952496	8.610791	8.734822	8.726797	8.07
1.212101	4.524726	33.44798	42.93577	4.250978	67.47234	2.680738	5.631827	5.477982	4.899955	5.25
0.592217	9.266919	38.1537	34.47923	13.59404	22.08846	1.924417	7.11212	6.978252	7.102731	6.97
2.023911	12.23992	39.51004	38.35115	6.374477	30.72848	0.852287	12	11.37778	11.57226	12.39
1.756698	5.589852	31.36824	28.4464	8.60974	89.84091	0.268322	6.839196	6.856746	6.897592	6.81
0.628697	10.47469	18.16909	28.84578	13.69061	3.274189	2.636277	11.18422	11.29852	11.22334	11.09
1.196616	4.02417	7.922525	25.81737	9.739332	10.37984	0.259554	6.623871	6.911623	6.543472	6.45

References

- [1] Li B, Guo Z, Zheng L, Qi B. A comprehensive review of wax deposition in crude oil systems: mechanisms, influencing factors, prediction and inhibition techniques. *Fuel*, 2024; 357: 129676. <https://doi.org/10.1016/j.fuel.2023.129676>
- [2] Kiyangi W, Guo J-X, Xiong R-Y, Su L, Yang X-H, Zhang S-L. Crude oil wax: a review on formation, experimentation, thermodynamic and kinetic modeling, prediction and remediation techniques. *Petroleum Science*, 2022; 19: 2343–2357. <https://doi.org/10.1016/j.petsci.2022.08.008>
- [3] Sousa AL, Matos HA, Guerreiro LP. Preventing and removing wax deposition inside vertical wells: a review. *Journal of Petroleum Exploration & Production Technology*, 2019; 9: 2091–2107. <https://doi.org/10.1007/s13202-019-0609-x>
- [4] Wen J. Progress in wax deposition characteristics and prediction methods for high pour point and viscous crude oil water system. *Processes*, 2025; 13(4): 1115. <https://doi.org/10.3390/pr13041115>
- [5] Elphingstone Jr GM, Greenhill KL, Hsu JJC. Modeling of multiphase wax deposition. *Journal of Energy Resources Technology-transactions of The Asme*, 1999;121: 81-85. <https://doi.org/10.1115/1.2795072>
- [6] Elkatory MR. Mitigation and remediation technologies of waxy crude. *Polymers*, 2022; 14(16): 3231. <https://doi.org/10.3390/polym14163231>
- [7] Amar MN, Singh S, Bahadur I, Hashemi H, Ramjugernath D. Predicting wax deposition using robust machine learning. *Results in Engineering*, 2022; 15: 100484. <https://doi.org/10.1016/j.rineng.2022.100484>.
- [8] Zhu H, Yu P, Li C, Yang F, Yao B, Yang S, Peng H. Wax deposition during the transportation of waxy crude oil: modeling and field implications. *Energy & Fuels*, 2024, 38(5), 2319–2332. <https://doi.org/10.1021/acs.energyfuels.3c04687>
- [9] Lal B, Bavoh CB, Sayani JKS Machine-learning in wax deposition: methodologies, numerical models, and artificial intelligence for flow assurance. In: *Machine Learning and Flow Assurance in Oil and Gas*, 2023, pp. 1–25.
- [10] Khalighi J. et al. Wax precipitation prediction using a novel intelligent method based on LS-SVM and genetic algorithm. *Journal of Petroleum Science & Engineering*, 2024. <https://doi.org/10.1016/j.petrol.2024.112376>
- [11] Ahmadi M. Data-driven approaches for predicting wax deposition. *Energy*, 2023, 265, 126296. <https://doi.org/10.1016/j.energy.2022.126296>
- [12] Obanijesu EO, Omidiora EO. Artificial neural network's prediction of wax deposition potential of Nigerian crude oil for pipeline safety. *Petroleum Science & Technology*, 2008; 26(15–16): 1977–1991. <https://doi.org/10.1080/10916460701399485>
- [13] Zhang Z, Shen Y, Zhang L, Xiao S, Jin X. A wax deposition prediction method for pumping oil wells based on LSTM neural networks. *Journal of Engineering Science and Technology Review*, 2023, 16(6), 177–184. <https://doi.org/10.25103/jestr.166.22>
- [14] Ridzuan N, Yaacob Z, Adam FW. Response surface methodology on wax deposit optimization. *Malaysian Journal of Analytical Sciences*, 2017; 21(2): 452–459. <https://doi.org/10.17576/mjas-2017-2102-21>.
- [15] Dehaghani AHS. An intelligent model for predicting wax deposition thickness during turbulent flow of oil. *Petroleum Science and Technology*, 2017; 35: 1706–1711. <https://doi.org/10.1080/10916466.2017.1358281>
- [16] Alnaimat F, Ziauddin M. Wax deposition and prediction in petroleum pipelines. *Journal of Petroleum Science and Engineering*, 2020; 184: 106385. <https://doi.org/10.1016/j.petrol.2019.106385>.
- [17] Eghtedaei R, Sasanipour J, Zarrabi H, Palizian M, Baghban A. Estimation of wax deposition in oil production units using an RBF-ANN strategy. *Petroleum Science and Technology*, 2017; 35: 1737–1742. <https://doi.org/10.1080/10916466.2017.1380043>
- [18] Nait Amar M, Ghahfarokhi AJ, Ng CSW. Predicting wax deposition using robust machine learning techniques. *Petroleum*, 2022; 8(2): 167–173. <https://doi.org/10.1016/j.petlm.2021.07.005>.
- [19] Xie Y, Xing Y. A prediction method for the wax deposition rate based on a radial basis function neural network. *Petroleum*, 2017; 3(2): 237–241. <https://doi.org/10.1016/j.petlm.2016.11.003>.

- [20] Obibuike UJ, Ekwueme ST, Ohia NP, Ukaeru FC, Onyejekwe IM, Udechukwu MC, Yahya HB. Modelling and optimisation of geothermal binary ORC systems using response surface methodology and artificial neural networks. *Zaštita Materijala*, 2026; 67(1): 14-35. <https://doi.org/10.62638/ZasMat1329>.
- [21] Jalalnezhad MJ, Kamali V. Development of an intelligent model for wax deposition in oil pipeline. *Journal of Petroleum Exploration and Production Technology*, 2016; 6(1): 129–133. <https://doi.org/10.1007/s13202-015-0160-3>.
- [22] Kim D, Park H, Lee S, Cho J. AI-based prediction of wax deposition characteristics in crude oil pipelines using experimental and sensor data. *Journal of Petroleum Science and Engineering*, 2022; 213: 110520. <https://doi.org/10.1016/j.petrol.2022.110520>
- [23] Chen Z. Modeling wax deposition rate in waxy crude oil pipelines using artificial neural networks. *Energy Reports*, 2024; 11: 458–470. <https://doi.org/10.1016/j.egyr.2024.01.065>.
- [24] Jin W, Zhang L, Li Q, Liu G. Artificial neural network modeling for prediction of wax deposition thickness from experimental flow-loop data. *Fuel*, 2023; 346: 128249. <https://doi.org/10.1016/j.fuel.2023.128249>.
- [25] Obaseki FA, Al-Majed A, Ahmed R. Dynamic modeling and ANN-assisted prediction of wax deposition in multiphase pipelines. *Journal of Energy Resources Technology*, 2021; 143(8): 083002. <https://doi.org/10.1115/1.4050019>.
- [26] Shehata SA, El-Metwally IM, Abdelgawad KF, Elkhawaga FA. Efficacy of agro-industrial wastes on the weed control, nutrient uptake, growth, and yield of onion crop (*Allium cepa* L.). *Journal of Soil Science and Plant Nutrition*, 2022; 22(2): 2707–2718. <https://doi.org/10.1007/s42729-022-00858-0>.
- [27] Khama ER, Loyibo EZ, Okologume W, Ekwueme ST, Okafor CV, Ohia NP. Investigation of the performance of activated carbon derived from ripe plantain peels for CO₂ capture: modelling and optimisation using response surface methodology. *Zaštita Materijala*, 2024, 65(2), 258–272. <https://doi.org/10.62638/ZasMat1329>
- [28] Obibuike UJ, Ekwueme ST, Ohia NP, Ukaeru FC, Onyejekwe IM, Udechukwu MC, Yahya HB. Modelling of drillstring hook loads for torque and drag evaluation in extended reach wells. *Petroleum & Coal*, 2025; 67(2): 540.
- [29] Salam KK, Arinkoola AO, Oke EO, Adeleye JO. Optimization of operating parameters using response surface methodology for paraffin-wax deposition in pipeline. *Petroleum & Coal*, 2014; 56(1): 19–28.
- [30] Adeyanju OA, Oyekunle LO. Optimization of wax deposition in sub-cooled pipeline using response surface methodology. In: *SPE Nigeria Annual International Conference and Exhibition*, 2015, SPE-178275. Society of Petroleum Engineers. <https://doi.org/10.2118/178275-MS>.
- [31] Elganidi I, Elarbe B, Ridzuan N, Abdullah N. Optimisation of reaction parameters for a novel polymeric additives as flow improvers of crude oil using response surface methodology. *Journal of Petroleum Exploration and Production Technology*, 2022; 12(2): 437–449. <https://doi.org/10.1007/s13202-021-01254-9>

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